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Dona Wells
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MT

Serial No.: 10/533096
Patent No.: 7,008,967 B2
Issued: March 7, 2006
Applicant(s): Martin Jokobus Keyser and
Margaretha Coertzen
Title: Production of Synthesis Gas and
Synthesis Gas Derived Products

Commissioner for Patents
P.O. Box 1450
Alexandria, VA 22313-1450

ATTN: DECISION AND CERTIFICATE OF CORRECTION
BRANCH OF THE PATENT ISSUE DIVISION

SECOND REQUEST FOR CERTIFICATE OF CORRECTION OF PATENT
FOR PTO MISTAKE (37 CFR §1.322 (a))

Sir:

Attached is a copy of the original Certificate of Correction dated August, 2006. It is respectfully requested that a second Certificate of Correction be issued for the patent identified in the heading. The first issued Certificate of Correction contained errors that occurred through the fault of the Patent Office. The original Request for Certificate of Correction, copy attached, was three pages. The middle page of the COC (page 2) was entirely omitted.

Please send the certificate to:

Clement H. Luken, Jr.
Wood, Herron & Evans, L.L.P.
2700 Carew Tower
Cincinnati, Ohio 45202

Certificate
SEP 25 2006
of Correction

If there is any further charge or credit due, please use Deposit Account No. 23-3000.

Respectfully submitted,

WOOD, HERRON & EVANS, L.L.P.

By:

Clement H. Luken, Jr.
Clement H. Luken, Jr., 32,742

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SEP 27 2006

UNITED STATES PATENT AND TRADEMARK OFFICE
CERTIFICATE OF CORRECTION

PATENT NO. : 7,008,967 B2
APPLICATION NO. : 10/533096
DATED : March 7, 2006
INVENTOR(S) : Martin Jokobus Keyser and Margaretha Coertzen

Page 1 of 1

It is certified that error appears in the above-identified patent and that said Letters Patent is hereby corrected as shown below:

Column 1, line 41, reads "...methane obviating the need to quench the raw synthesis gas..." and should read -- ...methane, obviating the need to quench the raw synthesis gas... --.

Column 1, line 56, reads "Subjecting the steam at a temperature of at least 400° C., ..." and should read -- Subjecting the upgraded synthesis gas to a water-gas shift reaction stage typically includes adding steam at a temperature of at least 400° C.,... --.

Column 2, lines 36-37, reads "The Fischer-Tropsch hydrocarbon synthesis stage may be provided with any bed reactor. The pressure in the reactor..." and should read -- The Fischer-Tropsch hydrocarbon synthesis stage may be provided with any suitable reactor such as a tubular fixed bed reactor, a slurry bed reactor or an ebullating bed reactor. The pressure in the reactor...--.

Column 3, lines 12-13, reads "The invention will now be described, by way of example, with reference to the ..." and should read -- The invention will now be described, by way of example, with reference to the accompanying diagrammatic drawings in which --.

Column 12, line 1, reads "The process as claimed in claim 3, which the thermal ..." and should read -- The process as claimed in claim 3, in which the thermal ...--.

Column 12, lines 32-34, reads "The process as claimed in claim 11, the synthesis gas conversion stage is a Fischer-Tropsch hydrocarbon synthesis ge." and should read -- The process as claimed in claim 11, in which the synthesis gas conversion stage is a Fischer-Tropsch hydrocarbon stage. --.

Signed and Sealed this

Twenty-second Day of August, 2006



JON W. DUDAS
Director of the United States Patent and Trademark Office

UNITED STATES PATENT AND TRADEMARK OFFICE
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MAILING ADDRESS OF SENDER:

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Column 4, line 58, reads " $3C + 2H_2O \rightarrow CH_4 + 2CO \dots$ " and should read –
 $3C + 2H_2O \rightarrow CH_4 + 2CO \dots$ –.

Column 5, lines 62- 63, reads "In the synthesis gas sweetening stage 20, the cooled synthesis, gas is further cooled in a series of heat exchangers ..." and should read – In the synthesis gas sweetening stage 20, the cooled synthesis gas is further cooled in a series of heat exchangers ... –.

Column 6, lines 11-12, reads "...are removed from the synthesis gas sweetening stage 20 by means along the naphtha removal line 50." and should read – are removed from the synthesis gas sweetening stage 20 by means of the sulphur removal line 52, whilst the naphtha is passed to a refinery (not shown) along the naphtha removal line 50. –.

Column 7, lines 46-47, reads "... (trade name) conventional process being similar to the process 10 as far as the stages 20, 22, 24 and 26 are ..." and should read – ... (trade name) gasification process followed by quenching and cooling of raw synthesis with the conventional process being similar to the process 10 as far as the stages 20, 22, 24 and 26 are ... –.

Column 8, line 24, reads "Composition (mol %)" and should read – Composition (mole %) –.

Column 8, line 62, reads "... invention, as illustrated, also does no require a methane..." and should read – ... invention, as illustrated, also does not require a methane... –.

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